AMENDMENTS TO THE CLAIMS

The following listing of claims will replace all prior versions and listings of claims in the application.

LISTING OF CLAIMS

- 1. (currently amended) A solid catalyst for ethylene polymerization, which uses, as comprising a magnesium halide source, derived from a magnesium compound represented by a formula $(RMgX)_p(MgX_2)_q$, in which R is an alkyl group having from 3 to 12 carbon atoms, X is halogen, and the molar ratio of q to p is in the range of from larger than 0 to 1 between 0 and 1.
- 2. (currently amended) The solid catalyst for ethylene polymerization as claimed in of claim 1, characterized in that wherein the molar ratio of q to p is in the range of from 0.05 to 0.95.
- 3. (currently amended) The solid catalyst for ethylene polymerization as claimed in of claim 1, characterized in that wherein X in the magnesium compound is chlorine.
- 4. (currently amended) A process for preparing the catalyst for ethylene polymerization as claimed in of claim 1, characterized in that wherein said process comprises the steps of:
- (1) reacting powdered magnesium with an alkyl halide of formula RX in an ether solvent to form a magnesium compound having a structure represented by of formula $(RMgX)_p(MgX_2)_q$, in which R is an alkyl group having from 3 to 12 carbon atoms, X is halogen, and the molar ratio of q to p is in the range of from larger than 0 to 1 between

<u>0 and 1</u>, wherein the molar ratio of the powdered magnesium to the alkyl halide is from 1:1 to 1:3;

- (2) impregnating the magnesium compound onto silica carrier and drying to give silica loading the provide a magnesium compound-loaded silica support, wherein the silica is used in such an amount that per gram silica loads from 0.5 to 5.0 mmol of magnesium element;
- (3) reacting the silica loading the magnesium compound-loaded silica support as prepared in of step (2) with an alkyl halide of formula R¹X, in which R¹ is an alkyl group having from 3 to 12 carbon atoms and X is halogen, in an alkane solvent to give a product, wherein the alkyl halide is used in such an amount that the molar ratio of Mg in the magnesium compound to the alkyl halide is in the range from 1:1 to 1:10;
- (4) reacting the product obtained from step (3) with a titanium compound and an alkyl aluminum compound to form a main catalyst component, wherein the titanium compound has a structure represented by formula Ti(OR²)_mCl_{4-m}, [[where]] R² is an alkyl group having from 1 to 4 carbon atoms and m is from 0 to 4, and the titanium compound is used in such an amount that the molar ratio of the Mg in the magnesium compound to the Ti in the titanium compound is in the range from 1:0.15 to 1:2.5, and wherein the alkyl aluminum compound has a structure represented by formula R³_nAlCl_{3-n}, [[where]] R³ is an alkyl group having from 1 to 14 carbon atoms and n is from 1 to 3, and the alkyl aluminum compound is used in such an amount that the molar ratio of the Mg in the magnesium compound to the Al in the alkyl aluminum compound is in the range from 1:0.08 to 1:3; and

- (5) contacting the main catalyst component with a cocatalyst component to form the catalyst for ethylene polymerization, wherein the cocatalyst component is an organo-aluminum compound, and the molar ratio of the Ti in the main catalyst component to the Al in the cocatalyst component is in the range from 1:30 to 1:300.
- 5. (currently amended) The process according to claim 4, characterized in that wherein the molar ratio of q to p is in the range of from 0.05 to 0.95.
- 6. (currently amended) The process according to claim 4, characterized in that wherein X in the magnesium compound is chlorine.
- 7. (currently amended) The process according to claim 4, characterized in that wherein the ether solvent is aliphatic hydrocarbyl ethers, aromatic hydrocarbyl ethers or cyclic ethers.
- 8. (currently amended) The process according to claim 7, characterized in that wherein the ether solvent is diethyl ether, di-n-propyl ether, di-n-butyl ether, di-isobutyl ether, diphenyl ether, methyl phenyl ether, tetrahydrofuran, or mixture thereof.
- 9. (currently amended) The process according to claim 4, characterized in that wherein the organo-aluminum compound is triethyl aluminum, diethyl aluminum chloride, triisobutyl aluminum, tri-n-hexyl aluminum, or mixture thereof.

- 10. (currently amended) The process according to claim 4, characterized in that wherein the alkyl halide of formula RX and formula R¹X is an alkyl chloride.
- 11. (currently amended) The process according to claim 10, characterized in that wherein the alkyl halide of formula RX and formula R¹X is independently chloropropane, chloro-n-butane, isobutyl chloride, isopentyl chloride or mixture thereof.
- 12. (currently amended) The process according to claim 4, characterized in that wherein the titanium compound is titanium tetrachloride, tetrabutyl titanate, methoxy titanium trichloride, butoxy titanium trichloride, or mixture thereof.
- 13. (currently amended) The process according to claim 4, characterized in that wherein the alkyl aluminum compound is triethyl aluminum, triisopropyl aluminum, triisobutyl aluminum, tri-n-hexyl aluminum, tri-n-octyl aluminum, tri(2-ethylhexyl) aluminum, diethyl aluminum chloride, ethyl aluminum dichloride, diisopropyl aluminum chloride, ethyl aluminum sesquichloride, or mixture thereof.
- 14. (currently amended) The process according to claim 4, characterized in that wherein the alkane solvent is an paraffin hydrocarbon.

- 15. (currently amended) The process according to claim 14, eharacterized in that wherein the alkane solvent is isopentane, hexane, n-heptane, octane, nonane, decane, or mixture thereof.
- 16. (currently amended) A process for preparing the catalyst for ethylene polymerization as claimed in of claim 1, characterized in that wherein said process comprises the steps of:
- (1) reacting powdered magnesium with an alkyl halide of formula RX in an ether solvent to form a magnesium compound having a structure represented by of formula $(RMgX)_p(MgX_2)_q$, in which R is an alkyl group having from 3 to 12 carbon atoms, X is halogen, and the molar ratio of q to p is in the range of from larger than 0 to 1 between 0 and 1, wherein the molar ratio of the powdered magnesium to the alkyl halide is in the range from 1:1 to 1:3;
- (2) impregnating the magnesium compound onto silica carrier and drying to give silica leading the provide a magnesium compound-loaded silica support, wherein the silica is used in such an amount that per gram silica loads from 0.5 to 5.0 mmol of magnesium element;
- (3) reacting the silica loading the magnesium compound-loaded silica support as prepared in of step (2) with a titanium compound and an alkyl aluminum compound to give a product, wherein the titanium compound has a structure represented by formula Ti(OR²)_mCl_{4-m}, where R² is an alkyl group having from 1 to 4 carbon atoms and m is from 0 to 4, and the titanium compound is used in such an amount that the molar ratio of the Mg in the magnesium compound to the Ti in the titanium compound

is in the range from 1:0.15 to 1:2.5, and wherein the alkyl aluminum compound has a structure represented by formula R³_nAlCl_{3-n}, where R³ is an alkyl group having from 1 to 14 carbon atoms and n is from 1 to 3, and the alkyl aluminum compound is used in such an amount that the molar ratio of the Mg in the magnesium compound to the Al in the alkyl aluminum compound is in the range from 1:0.08 to 1:3;

- (4) reacting the product obtained from step (3) with an alkyl halide of formula R¹X, in which R¹ is an alkyl group having from 3 to 12 carbon atoms and X is halogen, in an alkane solvent to form a main catalyst component, wherein the alkyl halide is used in such an amount that the molar ratio of Mg in the magnesium compound to the alkyl halide is in the range from 1:1 to 1:10; and
- (5) contacting the main catalyst component with a cocatalyst component to form the catalyst for ethylene polymerization, wherein the cocatalyst component is an organo-aluminum compound, and the molar ratio of the Ti in the main catalyst component to the Al in the cocatalyst component is in the range from 1:30 to 1:300.
- 17. (currently amended) Use of the A polymerization process, comprising contacting ethylene and the catalyst as claimed in of claim 1 in the polymerization of ethylene.
- 18. (currently amended) The use as claimed in polymerization process of claim 17, characterized in that wherein the main catalyst component is suspended in a mineral oil to form a slurry for the polymerization of ethylene, and said main catalyst component comprises from 20 to 30 percent by weight of the slurry.